Zeolite Y from rice husk ash encapsulated with Ag-TiO$_2$: characterization and applications for photocatalytic degradation catalysts

R.M. Mohamed$^{a,b,*}$, I.A. Mkhalid$^a$, M. Abdel Salam$^a$, M.A. Barakat$^{b,c}$

$^a$Chemistry Department, Faculty of Science, King Abdulaziz University, P.O Box 80203, Jeddah 21589, Saudi Arabia
Tel. +966 540715648; Fax: +966 2 6952292; email: imkhalid@kau.edu.sa

$^b$Advanced Materials Department, Central Metallurgical R&D Institute, CMRDI, P.O. Box 87, Helwan, Cairo, Egypt

$^c$Department of Environmental Sciences, King Abdulaziz University, Jeddah, Saudi Arabia

Received 24 December 2012; Accepted 9 February 2013

**ABSTRACT**

A high level of efficiency in the photocatalytic reactions was achieved by increasing the surface area of the photocatalyst by supporting fine TiO$_2$ particles on porous materials. Among various supports, zeolites seem to be an attractive candidate. Ti-incorporated Y zeolite was prepared by an ion-exchange method, while Ag was immobilized on the encapsulated titanium via impregnation method. The produced samples were characterized using X-ray diffraction, ultraviolet and visible spectroscopy, photoluminescence emission spectra, scanning electron microscopy, and surface area measurement. Furthermore, the catalytic performances of Ti-Ag/NaY tests were carried out for degradation of cyanide using visible light. The results reveal a good distribution of Ag on the zeolite. Ag doping can eliminate the recombination of electron-hole pairs in the catalyst. These results demonstrate that the optimum weight% of Ag to Ti-NaY is 0.3%; this weight% facilitates high performance by the photocatalyst, degrading 99% of cyanide in a 100 mg/L solution in 60 min.

**Keywords:** Rice husk ash; Ion-exchanged zeolite; Cyanide

1. Introduction

Zeolites are widely used in a range of applications from simple ion-exchange processes to gas separations [1,2]. Zeolites can also serve as catalysts, often after metals have been introduced into a framework, which brings about some special properties for heterogeneous catalysis [3]. The noncorrosive, environmentally-friendly, economically-viable nature of the zeolite-catalyzed reactions and their inherent capabilities of product selectivity have provided the opportunity for the development of various zeolites-based industrial processes. The metal, ion-exchanged NaY zeolite is one of the most important catalysts, because of its many properties, including activity, thermostability, reusability, easy handling, and easy preparation. Generally, the physicochemical properties of zeolites depend on the number of tetrahedrally coordinated Al atoms in the zeolite framework. Therefore, in order to improve the physicochemical properties of zeolites, isomorphous substitution of
framework Al by various metals, such as Ga, Fe, B, V, Zn, and Ti, has been widely studied [4–6].

TiO$_2$ is currently considered the most promising catalyst for the photocatalytic degradation of organic compounds, owing to its suitable band gap energy for redox reactions, mechanical and chemical stability, low cost, and convenience of preparation [7–10]. Given the current concern regarding environmental issues, it is anticipated that applications for TiO$_2$ will grow at increasing speed; in particular, urgent improvement of the TiO$_2$ photocatalytic degradation is needed for large-scale industrial treatment processes, such as wastewater treatment and de-NOx. From the green chemistry viewpoint, the photocatalytic decomposition of organic compounds in wastewater has attracted a great deal of attention [11–22]. The TiO$_2$ is one of the most effective photocatalysts because it is generally biologically and chemically inert, and is photostable with near-UV band gap energy. The fine TiO$_2$ powder, or crystals, can be dispersed in the water, in order to be clarified by irradiation; however, they must be removed by filtering after reaction, which is troublesome and costly. Thus, in order to solve this problem, many researchers have examined methods of fixing TiO$_2$ on other supporting materials, including glass beads [20–22], fiberglass [23–25], silica [26,27], an electrode [28], and zeolite [29,30]. Recently, some researchers have used zeolite as hosts to fix semiconductors, due to its unique, uniform pores and channel size. Since encapsulation of TiO$_2$ into zeolite was first introduced by Krueger et al. [31] and Liu et al. [32,33], many other encapsulation methods [34–37] have been developed to produce small particle sizes exhibiting quantum size effects or some improved photochemical reactions.

Pursuant to this goal, we describe the preparation and catalytic activity of a new photocatalyst. Degradation of cyanide under visible light in water was synthesized by introducing titania into the pores of zeolite (NaY) through the ion-exchange method, while Ag was immobilized on the encapsulated titanium via the impregnation method. This method is environmentally attractive because the authors convert rice husk ash (RHA) (waste materials) into zeolite materials (applicable materials). The rationale behind adding Ag was to increase the lifetime of e–h recombination and convert the absorbance of Ti-NaY from UV to the visible region.

2. Experimental details

2.1. Materials

Hydrochloric acid (37%) was purchased and then used in the procedure, as it was received (Aldrich). Sodium hydroxide pellets (Sigma–Aldrich, 99.5%) and sodium aluminate (Riedle-de Haen, 54% Al$_2$O$_3$, 41% Na$_2$O) were used. All the reagents were used as received. All aqueous solutions were prepared using doubly distilled water.

2.2. Preparation of zeolite

Initially, any dirt and soil attached to RH can be removed by washing with plenty of tap water and rinsing with distilled water. The metallic impurities in RH can be reduced to negligible levels by refluxing with hydrochloric acid (32%) [38]. The chemical composition of RHA, which was examined by X-ray fluorescence spectroscopy (XRF: Philips, PW1400), is shown in Table 1. We directly extracted the silica by stirring the acid-treated RH (after drying) with sodium hydroxide solution (4 M). During this process, silica was extracted in the form of sodium silicate together with other organic moieties, according to the method patented by Adam and Fua [39]. The sodium silicate obtained was converted to silica by adding suitable amounts of mineral acid. RHA was obtained by pyrolyzing the RH, at temperatures ranging from 500 to 800°C, for 5–6 h in a muffle furnace (Carbolite), in order to remove the organic contents. The yield of silica in this sample ash was 89%. In 2006, Chandrasekhar et al. [40] studied the effect of acid treatment, calcination temperature, and the rate of heating of RH; they showed that these parameters influenced the surface area, reactivity toward lime, and brightness of the ash. NaY zeolite was synthesized with two different gels (seed gel and feedstock gel); the difference between the two aforementioned gels is that the feedstock gel was prepared and used immediately without an aging step. The seed gel (Al$_2$O$_3$:10 SiO$_2$) was prepared first by adding the Na$_2$SiO$_3$ solution into the sodium aluminate (Riedle-deHaen 54% Al$_2$O$_3$, 41% Na$_2$O) solution, stirring until homogenous, and then leaving the solution undisturbed for 24 h at room temperature. The feedstock gel (Al$_2$O$_3$: 10 SiO$_2$) was prepared the same way, but

<table>
<thead>
<tr>
<th>Chemical compositions of RHA determined by XRF</th>
</tr>
</thead>
<tbody>
<tr>
<td>Chemical compositions of RHA</td>
</tr>
<tr>
<td>SiO$_2$</td>
</tr>
<tr>
<td>Al$_2$O$_3$</td>
</tr>
<tr>
<td>Fe$_2$O$_3$</td>
</tr>
<tr>
<td>K$_2$O</td>
</tr>
<tr>
<td>CaO</td>
</tr>
<tr>
<td>C</td>
</tr>
</tbody>
</table>
was used immediately without aging. The seed gel was then mixed into the feedstock gel, through vigorous stirring, until a homogeneous gel was obtained. The resulting gel remained at ambient temperature for 24 h, and crystallized at 110˚C for another 24 h. The final product was filtered, washed, and dried at 100˚C in an oven.

2.2. Insertion of TiO2 nanoparticles into zeolite Y

We employed a conventional, ion-exchange method, using an aqueous solution of 0.03 M potassium titanooxalate. One gram of NaY was added to the potassium titanooxalate solution and stirred for 24 h. After the ion-exchange, the zeolite sample was filtered, washed with doubly distilled water, in order to prevent the physically adsorbed titanium species from aggregating on the external surface of the zeolite, and then dried for 24 h in an oven at 100˚C. The resulting TiO2-exchanged zeolite (Ti-NaY) was calcined at 550˚C for 5 h, with a heating rate of 5˚C/min. The wt.% of Ti to zeolite Y was controlled at 5 wt.% for all prepared samples.

2.3. Preparation the Ag/Ti-NaY catalyst

Incipient wetness impregnation was used to introduce different wt.% Ag onto already formed Ti-NaY. Impregnation of Ag onto Ti-NaY was carried out as follows: AgNO3 was dissolved in 100 ml of deionized water and stirred. Then, a predetermined amount of Ti-NaY was stirred for 24 h at room temperature, evaporating by using an oil bath rotary evaporator. The obtained catalyst was dried for 24 h at 100˚C and then calcined at 500˚C for 5 h, with a heating rate of 5˚C/min. The Ag/Ti-NaY was labeled according to the different Ag ions loading on Ti-NaY, including: 0.1% Ag/Ti-NaY, 0.2% Ag/Ti-NaY, 0.3% Ag/Ti-NaY and 0.4% Ag/Ti-NaY.

2.4. Material characterization

X-ray diffraction (XRD) patterns were recorded using a Bruker axis D8 diffractometer with Cu Kα radiation (λ = 1.540 Å) over a 2θ collection range of 4–60°. Surface morphology of the catalyst was examined using scanning electron microscopy (SEM) JEOL 5,410 (Japan). Nitrogen adsorption and desorption isotherms were measured at −196˚C, using a Nova 2000 series Chromatech apparatus. All the samples were degassed at 200˚C for 2 h prior to data collection. Band-gab values of the samples were obtained via the UV–Visible diffuse reflectance spectra (UV–Vis-Diffuse reflectance spectra), in air at room temperature, in the wavelength range of 200–800 nm, using a UV/Vis/Near infrared spectrophotometer (V-570, JASCO, Japan). Photoluminescence (PL) emission spectra were recorded with the fluorescence spectrophotometer, Shimadzu RF-5301.

2.5. Photocatalytic tests

For liquid-phase photocatalytic degradation, the photocatalyst was dissolved in 300 ml of distilled water and 100 ppm of a potassium cyanide (KCN) solution (pH = 10.5, in order to avoid the evolution of hydrogen cyanide gas ), which was adjusted by an ammonia solution. These were placed in a horizontal cylinder annular batch reactor, irradiated with a blue fluorescent lamp (150 W, maximum energy at 450 nm), and doubly covered with a UV cut filter. The intensity data of UV light were confirmed to be under the detection limit (0.1 mW/cm2) of a UV radiometer. The reaction was carried out isothermally, at 25˚C, and samples of the reaction mixture were taken at different intervals for a total reaction time of one hour. The CN−[aq] concentration in the samples was estimated by volumetric titration with AgNO3, using potassium iodide to determine the titration endpoint [41]. The removal efficiency of CN−[aq] was measured by applying the following equation:

\[
\text{% Removal efficiency} = \left( \frac{C_0 - C}{C_0} \right) \times 100
\]

where C0 is the initial concentration of uncomplexed CN−[aq] in solution and C is the concentration of unoxidized CN−[aq] in solution.

3. Results and discussion

3.1. XRD analysis

Powder XRD is the most suitable analysis to characterize the crystalline structure of the catalyst particles, in order to indicate the effect of Ti and Ag loadings on the structure of zeolite Y. Fig. 1 depicts the XRD patterns pertaining to NaY, Ti-NaY, and Ag/Ti-NaY, showing that the crystallinity of zeolites were found to be unaltered after the ion-exchange process and impregnation method. Actually, the above-prepared Ti-exchanged zeolite sample and Ag/Ti-NaY do not contain an amorphous phase or TiO2 and Ag2O phase. This indicates that the structural damage is negligible during the ion-exchange process; it also indicates that the TiO2 particles
residing in the zeolite cavities or channels were too small to be detected by XRD. There were no peaks for the Ag₂O species, which indicated a good distribution of Ag on the zeolite.

3.2. UV–Vis

The UV–Vis diffuse reflectance spectra of the bulk TiO₂ and titanium-exchanged zeolite catalyst are displayed in Fig. 2. A significant blue shift of the spectrum was observed, when compared with that of bulk titania. This shift can be attributed to two factors.

First, it can be dependant on the size quantization effect. Due to the presence of extremely small Ti-oxide particles and/or the bands in the wavelength regions (330–370 nm), their intensity increases with an increase of Ti content. This result was in agreement with Easwaramoorthi and Natarajan [42]. The sudden fall in the wavelength indicated the presence of an optical band gap after the ion exchange of Ti species into the zeolite [43]. These observations proved the success of the ion-exchange process, despite the lack of a diffraction peak, attributed to TiO₂ observed in the XRD analysis. On the other side, the loading of Ag ions into the Ti-NaY caused a red shift toward a higher wavelength, from 400 to 520 nm for different loadings of Ag, when compared to Ti-NaY, which had a wavelength of about 390 nm. The direct band gap energies for the bare TiO₂, TiO₂ encapsulated into NaY, and Ag/Ti-NaY were calculated from their reflection spectra, based on a method suggested by Kumar et al. [44], and are shown in Table 2. It is clear that the energy gap decreased with an increase in the Ag ions, up to 0.3 wt.%. Also, at higher concentrations of Ag ions (i.e., 0.4 wt.%), no significant decrease in the energy gap was observed. This observation indicated that there was an optimum value for the doping of the Ag ion; above this optimum loading value the optical gap showed no more direct dependence on the metal ions [45].

3.3. PL characteristics

PL emission spectra have been used to study the transfer of the photogenerated electrons and holes, and to understand the separation and recombination of photogenerated charge carries. In order to investigate the photoelectric properties of the prepared samples, the PL spectra were detected for the different samples exited at 300 nm at room temperature, as shown in Fig. 3. It is clear that the position of emission of Ti-NaY is different from Ag/Ti-NaY samples,
and that Pl intensity greatly decreased with the increase of the Ag percent. Ag acts as a trapping site, to capture photogenerated electrons from TiO₂ conduction band, separating the photogenerated electron–hole pairs.

3.4. Structural analysis

The BET surface areas of the NaY, Ti-NaY, and Ag/Ti-NaY are tabulated in Table 3. A slight reduction in the $S_{\text{BET}}$ value was observed for NaY (from 716.6 to 704.3 m²/g then reduced to 685.4 m²/g after ion exchanged with zeolite), and subsequently with 0.4% Ag. This significant reduction in the surface area, after the loading of both titanium oxide and Ag ions, is good evidence of successful loading of TiO₂ and Ag through the ion-exchange and impregnation methods, respectively. In addition, pore mouth blockage, which is the most worrying phenomenon in the production of a supported zeolite catalyst, was not observed in the analysis.

<table>
<thead>
<tr>
<th>Sample</th>
<th>$S_{\text{BET}}$ (m²/g)</th>
<th>$V_p$ (cm³/g)</th>
</tr>
</thead>
<tbody>
<tr>
<td>NaY</td>
<td>716.6</td>
<td>0.350</td>
</tr>
<tr>
<td>Ti-NaY</td>
<td>704.3</td>
<td>0.345</td>
</tr>
<tr>
<td>0.1% Ag/Ti-NaY</td>
<td>700.0</td>
<td>0.340</td>
</tr>
<tr>
<td>0.2% Ag/Ti-NaY</td>
<td>695.5</td>
<td>0.328</td>
</tr>
<tr>
<td>0.3% Ag/Ti-NaY</td>
<td>687.3</td>
<td>0.305</td>
</tr>
<tr>
<td>0.4% Ag/Ti-NaY</td>
<td>685.4</td>
<td>0.299</td>
</tr>
</tbody>
</table>

The pore volume of the catalyst was found to slightly decrease from 0.350 cm³/g for NaY to 0.345 cm³/g for Ti-NaY. This reduction in pore volume was due to the agglomeration of TiO₂ clusters inside the pores of zeolite after the calcination step. Fig. 4 shows N₂ adsorption–desorption isotherm of 0.3% Ag/Ti-NaY photocatalyst. The results reveal that the type of isotherm is type IV. The micrograph structures of the NaY, Ti-NaY, and 0.3% Ag/Ti-NaY are seen in Fig. 5. The SEM results of the modified zeolites were in agreement with the XRD results, as there was no major change in the structure. The zeolite was able to keep its crystal shape, even after the loading of Ti species and Ag ions, as is shown in Fig. 4, respectively.

![Fig. 3. Pl spectra of Ti-NaY and Ag/Ti-NaY samples.](image)

![Fig. 4. N₂ adsorption–desorption isotherm of 0.3% Ag/Ti-NaY photocatalyst.](image)

![Fig. 5. Surface morphology of (A) NaY, (B) Ti-NaY, and (C) 0.3% Ag/Ti-NaY.](image)
On the other hand, the results of Energy-dispersive X-ray Spectroscopy (EDAX/EDX) analysis, which identify only the surface element of the sample, are shown in Fig. 6. It is clear, in examining (Fig. 6), that there was no specific signal for TiO₂ detected on the surface of the catalyst. As a result, we determined that the titanium oxide was successfully encapsulated inside the supercages of zeolite, through the ion-exchange method. This finding was in agreement with a few earlier studies. For example, Easwaramoorthi and Natarajan [42] did not detect any Ti presented on the external surface of zeolites in the case of TiO₂ encapsulated into zeolite by the ion-exchange method. However, they detected the presence of Ti on the surface of a zeolite loaded with TiO₂ that was prepared using the sol gel method. As such, the preparation method plays an important role in characteristics of the final material. For the case of Ag loaded on Ti-NaY as shown in Fig. 6, a small amount of Ag ions was detected to present on the surface of the catalyst. This result proved the successful loading of Ag ions through the impregnation method.

The morphology of 0.3%Ag/Ti-NaY was examined further using TEM imaging, as shown in Fig. 7. The TEM image confirmed the presence of Ag deposits on the surface of Ti-NaY. As is shown in Fig. 7, Ag deposits were well dispersed on many of the Ti-NaY particles; diameters ranged from 3 to 5 nm.

4. Photocatalytic tests

Highly dispersed Ag ions that were included within Ti-exchanged zeolite cavities were prepared using the impregnation method, which acted as the photocatalyst for a series of experiments on cyanide removal efficiency. The estimated data are summarized in Fig. 8. The results indicate that Ti-NaY and TiO₂ have no photocatalytic activity under visible light, due to their absorbance on the UV region. Additionally, an increase of wt.% from 0.1 to 0.3 lead to a high cyanide removal efficiency of 66–99%, respectively. No significant increase in photocatalytic activity was observed and higher concentrations of Ag ions (i.e. 0.3 wt.%) were used.

Photocatalytic activity is known to be dependent on the crystallinity, surface area, and morphology. It may be improved by slowing the recombination of photogenerated electron-hole pairs, extending the excitation wavelength to a lower energy range, and increasing the amount of surface-adsorbed reactant species. In general, the process for photocatalysis begins when supraband gap photons are directly absorbed, which generates electron-hole pairs in the semiconductor particles. This is followed by diffusion of the charge carriers to the surface of the particle, where the interaction with water molecules produces a highly reactive species of peroxide (O₂⁻) and hydroxyl radical (OH⁻), which are responsible for the degra-
dation of adsorbed organic molecules. Step-reactions in the photocatalytic process leading to the degradation of CN\textsuperscript{-}/CO\textsubscript{0} are presented in the following sequence:

\[
\begin{align*}
\text{TiO}_2 + \text{hv} & \rightarrow e^- + h^+ \\
e^- (\text{Ag}) & \rightarrow e^- (\text{Ag}) \\
e^- + O_2(\text{ads}) & \rightarrow O_2 \\
2e^-_t + 2H^+ + O_2 & \rightarrow H_2O_2 \\
H_2O_2 + e^-_t & \rightarrow OH^- + OH^+ \\
H^+ + H_2O & \rightarrow H^+ + OH^- \\
2CN^- + 4OH^- & \rightarrow 2N_2 + 2CO_2 + 2H_2 
\end{align*}
\]

5. Conclusions

The results of the current research underscore the considerable variation in photoactivity of TiO\textsubscript{2} phases when they are encapsulated on zeolites. The results presented above clearly demonstrate that the preparation of nanosized TiO\textsubscript{2} particles inside zeolites can be formed via ion exchange of the zeolite. The same observations were also obtained by incorporating Ag ions on Ti-NaY, using the impregnation method.

Overall, a significant photocatalytic rate enhancement is observed in the reaction studied. These findings were also investigated using XRD, UV–Vis, and EDX analyses. The Ag/Ti-NaY photocatalyst is a promising catalyst, due to its high removal efficiency of the pollutant under visible light. These results demonstrate the successful loading of Ag ions through the impregnation method. The maximum degradation efficiency achieved was 99\% at 0.3\% Ag/Ti-NaY after a 60 min reaction time. The doping of the Ag ion into the Ti-NaY was useful in improving the photocatalytic activity. This may be due to its ability to inhibit the e\textsuperscript{−}/h\textsuperscript{+} recombination, produced from the Ti species, inside the pores of zeolite. The new, heterogeneous photocatalyst Ag/Ti-NaY is a promising catalyst for cyanide degradation under visible light.

Acknowledgment

This project was funded by the Deanship of Scientific Research (DSR), at King Abdulaziz University, Jeddah, under grant number (1432/130/443). The authors thankfully acknowledge DSR technical and financial support.

References


