



Removal of Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions by the synthesized sodium dodecyl benzene sulphonate-based tin (IV) phosphate (SDBS-SnP) cation exchanger

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ABSTRACT

The newly synthesized cation exchanger sodium dodecyl benzene sulphonate (SDBS)-based tin (IV) phosphate, SDBS-SnP, has been found to be a good cation exchange material for the removal of Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions from water sample. The cation exchanger, SDBS-SnP, was synthesized and was characterized by using the physical techniques like infrared spectroscopy, X-rays diffraction (XRD), scanning electron microscopy and thermal and differential thermogravimetric analysis. The XRD studies indicated that the SDBS-SnP is an amorphous material. The elemental analysis of the material was also performed on the ion exchange material to ascertain the presence of surfactants and inorganic constituents. The ion exchange capacity is improved to a value of 2.20 milli equivalent of Na^+ ions per gram cation exchange material. The concentration behaviour showed that 1.0 M NaNO_3 was the optimum concentration for the complete removal of H^+ -ions from SDBS-SnP. The H^+ -ions were eluted by 160 mL of 1.0 M NaNO_3 solution. The ion exchange material retained more than 95% of its initial values of ion exchange capacity on heating to 100°C for an hour. The cationic exchanger is found to be highly selective for Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions, and can be used for the separation of Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions from the solution containing acid, alkalis or alkaline earth metals.

Keywords: Fibrous ion exchanger; Sn (IV) phosphate; Sodium dodecyl benzene sulphonate; SDBS-SnP; Adsorption studies; Water treatment

1. Introduction

The studies on the synthesis and ion exchange behaviour of composite materials comprising the surfactants and inorganic ion exchange materials have gained popularity in the recent years [1–7]. The

surfactant-based cation exchangers have been capable of exchanging and adsorbing the metal ions through the surfactant and inorganic constituents. The presence of surfactant molecules in the inorganic matrix enhanced the ion exchange capacity and also made the ion exchangers chemically and thermally more stable. The intercalation of surfactant molecules into

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the inorganic matrix makes the composite material environment friendly. The earlier studies [8–10] have shown that the surfactant–inorganic interaction is the result of direct co-condensation of anionic inorganic species with a cationic surfactant (S^+I^-), cooperative condensation of cationic inorganic species with an anionic surfactant (S^-I^+), condensation of ionic inorganic species with surfactants having the similar charge and the condensation mediated by the counter ions of opposite charge of surfactant headgroup ($S^+X^-I^+$ and $S^-M^+I^-$, where X^- denotes anions such as Cl^- or Br^- , and M^+ denotes cations like K^+ or Na^+). These nano-porous materials possessed the surface area in order of magnitude greater than nanoparticles and were capable of binding a broad range of ions/molecules [11,12]. They specifically adsorb heavy metals and were reported to be effective for the removal of mercury and other metals such as cadmium, silver and molybdenum from soil and sludge [13]. The charged headgroup of surfactant molecules removes metal ions by binding with oppositely charged ions through complexation effect, electron attraction and charge neutralization. The surfactant molecules reduce the interfacial tensions [14] between solid and liquid phases and, thereby, it helps to wet the surface properly and facilitates the exchange of metal ions easily and readily from the surface.

The present study describes the synthesis of surfactant based, cationic exchange material capable of exchanging and removing the heavy metal ions from water. It is environment friendly material because SDBS-SnP can be decomposed and recycled after its exhaustion. It presents better alternate for the resin-based or polymer-based ion exchange materials (as they are non-biodegradable in nature and pose environmental problem for its disposal). The ion exchange capacity, stability towards higher temperature and elution and adsorption behaviour of SDBS-SnP cation exchanger have been studied and discussed herewith.

2. Experimental

2.1. Reagents and chemicals

Tin (IV) chloride (CDH, India), cadmium (II) nitrate (CDH, India), magnesium (II) nitrate (CDH, India) and strontium (II) nitrate (CDH, India) were used during the experiment. Sodium dodecyl benzene sulphonate (SDBS, Merck-Schuchardt, Germany), calcium nitrate (Merck-Schuchardt, Germany), barium nitrate (Merck-Schuchardt, Germany), nickel nitrate (Merck-Schuchardt, Germany) and sodium nitrate (Merck-Schuchardt, Germany) were used as obtained

from supplier. Phosphoric acid, copper (II) nitrate and lead (II) nitrate were obtained from Qualigens (India) and mercuric (II) nitrate and zinc (II) nitrate were obtained from Thomas Baker. All other reagents used were of Anal R grade. Doubly distilled demineralized water with specific conductance, $1\text{--}2 \times 10^{-6} \Omega^{-1} \text{cm}^{-1}$, was used during the experiments.

2.2. Instruments used

The X-ray diffraction was performed on a Philips Analytical X-ray B.V. diffractometer (type PW 170 B. V. The Netherlands) and infrared spectroscopy (IR) spectrum was recorded on Shimadzu 8201 PC spectrophotometer (Japan). The elemental analysis was done by Heraeus Carlo Erba-1108 analyzer (Italy). Differential pulse polarogramme was recorded by using an Elico CL-362 Pulse Polarograph (India) and scanning electron microscopy (SEM) studies were performed on SEM Hitachi-S520, Japan. The thermal and differential thermogravimetric analysis (TGA/DTA/DTG) curves were recorded on Perkin Elmer Pyris Diamond (USA).

2.3. Preparation of the reagent solutions

The stock solutions of 0.1 M SDBS, 0.6 M solution of phosphoric acid, 0.1 M sodium hydroxide, 1.0 M sodium nitrate, 0.01 M cadmium nitrate, 0.01 M lead nitrate, 0.01 M zinc nitrate, 0.01 M copper nitrate, 0.1 M sodium nitrate, 0.1 M magnesium nitrate, 0.1 M potassium nitrate and 0.1 M calcium nitrate were prepared in the doubly distilled water. Solution of tin (IV) phosphate was prepared by adding tin (IV) chloride to 0.6 M H_3PO_4 .

2.4. Synthesis of the ion exchange material

Samples of sodium dodecyl benzene sulphonate-tin (IV) phosphate (SDBS-SnP) were prepared by adding one volume of 0.30 M tin (IV) chloride solution to two volumes of a (1:1) mixture of 0.60 M H_3PO_4 and SDBS solutions drop-wise with the constant stirring by using a magnetic stirrer at room temperature. The resulting slurry was stirred for 3.5 h at room temperature, filtered and then washed with demineralized water till pH ~ 4 was achieved. The samples were then left to dry at room temperature. The dried material was having the sheet-like structure. It was then crushed into small pieces. The synthesized material was kept in 1.0 M HNO_3 for 24 h to change it in the form of H^+ form. After keeping in HNO_3 , it was filtered, washed with doubly distilled water several times to remove the residual H^+ ions completely. The material in H^+ -form was left to

dry at 45°C for a day and then sieved to obtain particles of size 50–70 mesh. Then, the ion exchange capacity of the various synthesized samples was determined by column process, and it was found that the sample-3 possessed the highest ion exchange capacity and, therefore, it was selected for further studies.

2.5. Ion exchange capacity concentration behaviour and elution behaviour

To determine the number of ionogenic groups present in the synthesized exchanger, 1.0 g of the material (in the H⁺-form) was taken in a glass burette of internal diameter ~1 cm and fitted with glass wool at the bottom. 250 mL of 1.0 M NaNO₃ solution was used as eluent, maintaining a slow flow rate (~0.5 mL min⁻¹). The effluent was titrated against 0.1 M NaOH solution using phenolphthalein as an indicator to determine the total H⁺-ions liberated during ion exchange process.

The optimum concentration of eluent needed to complete elution of H⁺ ions was determined by passing a fixed volume (250 mL) of different concentrations of NaNO₃ solution containing 1.0 g of the ion exchange material kept in a column. The H⁺-ions eluted out were titrated against a standardized 0.1 M NaOH solution using phenolphthalein as an indicator. To determine the elution behaviour of the material, the above experiment was repeated in which 1.0 g of the cation exchanger was taken in a column and eluted with 1.0 M NaNO₃ solution. The effluents were collected in different 10 mL fractions and the liberated H⁺ ions were determined by titrating against 0.1 M NaOH solution using phenolphthalein as an indicator. The above experiments were repeated at least 3–4 times and the observed results were found to be reproducible within ±5%.

2.6. Thermal stability

The thermal stability of the cation exchanger was determined by taking several 1.0 g samples of SDBS-SnP and heating them at different temperatures e.g. 100, 150, 200 and 300°C in a muffle furnace for an hour. After cooling to room temperature, their ion exchange capacity was determined.

2.7. Adsorption studies

The adsorption behaviour of SDBS-SnP was determined by taking 200 mg of the synthesized material in H⁺-form in a conical flask containing 20.0 mL of metal nitrate solutions (1.0 × 10⁻³ M). The conical flask was thermostated at room temperature (25.0 ± 0.5°C) for 24 h, with shaking intermittently to achieve equilib-

rium. The concentration of the metal ions was determined before and after the equilibrium was achieved. The concentrations of Hg²⁺, Ni²⁺, Ba²⁺, Mg²⁺, Ca²⁺ and Sr²⁺ ions were determined by titration with standardized disodium salt of EDTA solution [15]. The concentrations of Cu²⁺, Cd²⁺, Pb²⁺ and Zn²⁺ ions were determined by measuring the diffusion current [16]. The concentration of Fe²⁺ was determined by spectrophotometric method using hydroxyl amine, sodium acetate and 1,10-phenanthroline. Iron(II) gave a complex having orange-red colour with λ_{max} at 510 nm. The absorbance of the solution was recorded before and after achieving the equilibrium at 510 nm wavelength.

The distribution coefficient (K_d) for these metal ions was calculated by using the following relationship:

$$K_d = \frac{I - F}{F} \frac{V}{M} \text{ (mL g}^{-1}\text{)}$$

where K_d = distribution coefficient (mL g⁻¹), I = initial amount of metal ions in the solution, F = final amount of metal ions in the solution, V = volume of the solution (mL), M = amount of the exchanger taken (g).

2.8. Metal ions separations

The binary separations for metal ions were carried out by column method. 2.0 g of the synthesized material was taken into the column with internal diameter ~0.6 cm. The column was washed thoroughly with the doubly distilled water and then the mixture containing Hg²⁺-Ni²⁺, Hg²⁺-Ba²⁺, Hg²⁺-Mg²⁺ and Hg²⁺-Sr²⁺ to be separated was loaded onto it, maintaining a flow rate of ~12–15 drops min⁻¹. The separation was achieved by passing a suitable solvent through the column as eluent and the metal ions in the effluent were determined quantitatively by EDTA titrations. Quaternary separations for Cu²⁺, Cd²⁺, Pb²⁺ and Zn²⁺ ions were carried out using a column with internal diameter ~0.6 cm containing 2.0 g of the synthesized material. The column was washed thoroughly with the demineralized water and the mixture containing Cu²⁺, Cd²⁺, Pb²⁺ and Zn²⁺ ions was loaded onto it with a flow rate of ~12–15 drops min⁻¹. The separations for Cu²⁺, Cd²⁺, Pb²⁺ and Zn²⁺ ions before and after adsorption were determined by recording the differential pulse polarogramme.

2.9. Separation in presence of acid, alkali and alkaline earth metals

To study the effectiveness of SDBS-SnP for the removal of Cu²⁺, Cd²⁺, Hg²⁺ and Pb²⁺ ions in the

presence of acid, alkalis and alkaline earth metals, the above experiments were repeated by taking a mixture of Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions in the solutions containing 0.01 and 0.1M acid, alkalis or alkaline earth metals.

3. Results and discussion

The ion exchange capacity of the sample of ion exchange material synthesized with different amount of SDBS is given in Table 1. The ion exchange capacity increased from 1.50 (for Sn (IV) phosphate) to 1.63 meq/g for SDBS-SnP having 0.0001 M SDBS. The ion exchange capacity (i.e.c.) was highest for the sample (No. 3) having 0.001 M SDBS. At 0.01 M SDBS, the i.e.c. values decreased, may be due to the blocking of the some of the ion-exchanging site of tin (IV) phosphate by the surfactant molecules. Thus, the addition of surfactant to the tin (IV) phosphate ion exchanger increased the ion exchange capacity for the Na^+ ions from 1.50 to 2.20 meq/g [17]. The strength of the interaction between the ion exchange material and mobile ions is determined by the nature, ionic size and number of the charges on the metal ion and on the functional group of the ion exchanger. Ions that have a stronger ionic interaction require a higher salt concentration and elute later in the gradient. The elution behaviour of the cation exchanger for H^+ -ions reveals that the process of exchange is quite fast and almost all the H^+ ions were eluted out in the first 160 mL of the effluent from a column of 1.0 g exchanger (Fig. 1). At lower salt concentrations, H^+ -ions with the weak ionic interactions starts to elute first from the column and H^+ -ions that have a stronger ionic interaction require a higher salt concentration and elute later in the gradient. Thus, the optimum concentration of NaNO_3 required to remove H^+ ions completely from the exchanger was found to be 1.0 M (Table 2).

The study on variation on ion exchange capacity at different temperatures reveals that SDBS-SnP is thermally stable till it attains temperature $\sim 150^\circ\text{C}$, where the exchange capacity of 91.36% is retained by the material. On heating it further in the temperature

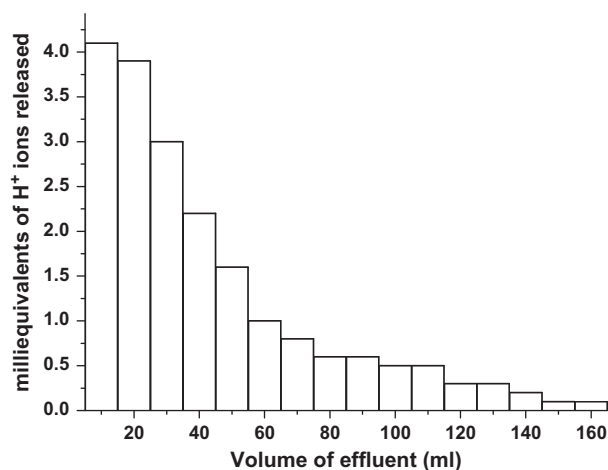


Fig. 1. Histogrammes showing the elution behaviour of SDBS-SnP.

Table 2

Variation in ion exchange capacity of SDBS-SnP cation exchanger with varying eluant concentrations

Concentration of NaNO_3 (M)	Ion exchange capacity (meq/g)
0.2	0.86
0.4	1.24
0.6	1.62
0.8	1.91
1.0	2.20
1.2	2.20

range $150\text{--}200^\circ\text{C}$, the ion exchange capacity is decreased to about 59.09%, may be due to the disruption in the bonding pattern of sulphonic part of SDBS from where the exchange of ions occurs. On heating to 300°C , the material possesses only 43.18% of ion exchange capacity of its initial value (i.e. before heating) may be due to exchange capacity of tin (IV) phosphate. The results are summarized in Table 3. The thermal behaviour of SDBS-SnP was further explored by thermogravimetric studies. The thermogravimetric and differential thermal analysis of SDBS-SnP show two-step mass losses, 11.4 and 7.9% up to the temperature 200°C with endo effect at 77°C which confirm the removal of external water molecules associated with the ion exchange material. The curves show 2.5 and 0.9% weight losses at 540°C due to thermal decomposition of SDBS and volatilization of alkyl part of SDBS [18]. A large weight loss of 19.1% was observed in the temperature range of $558\text{--}561^\circ\text{C}$ due to the decomposition in the residual part of SDBS (i.e. benzene sulphonate groups) and Sn (IV) phosphate

Table 1
Ion exchange capacity of various samples of SDBS-SnP

Sample number	SDBS used (moles)	Na^+ ion-exchanging capacity (meq/g)
Sample-1	0.0	1.50
Sample-2	0.01	1.03
Sample-3	0.001	2.20
Sample-4	0.0001	1.63

Table 3
Thermal stability and appearance of SBDS-SnP cation exchanger after heating at different temperatures for 1 h

Heating temperature (°C)	Na ⁺ -ion exchange capacity (meq/g)	Physical appearance	% Retention in ion exchange capacity
100	2.10	White	95.45
150	2.01	White shiny	91.36
200	1.30	Creamish white	59.09
300	0.95	Yellow	43.18

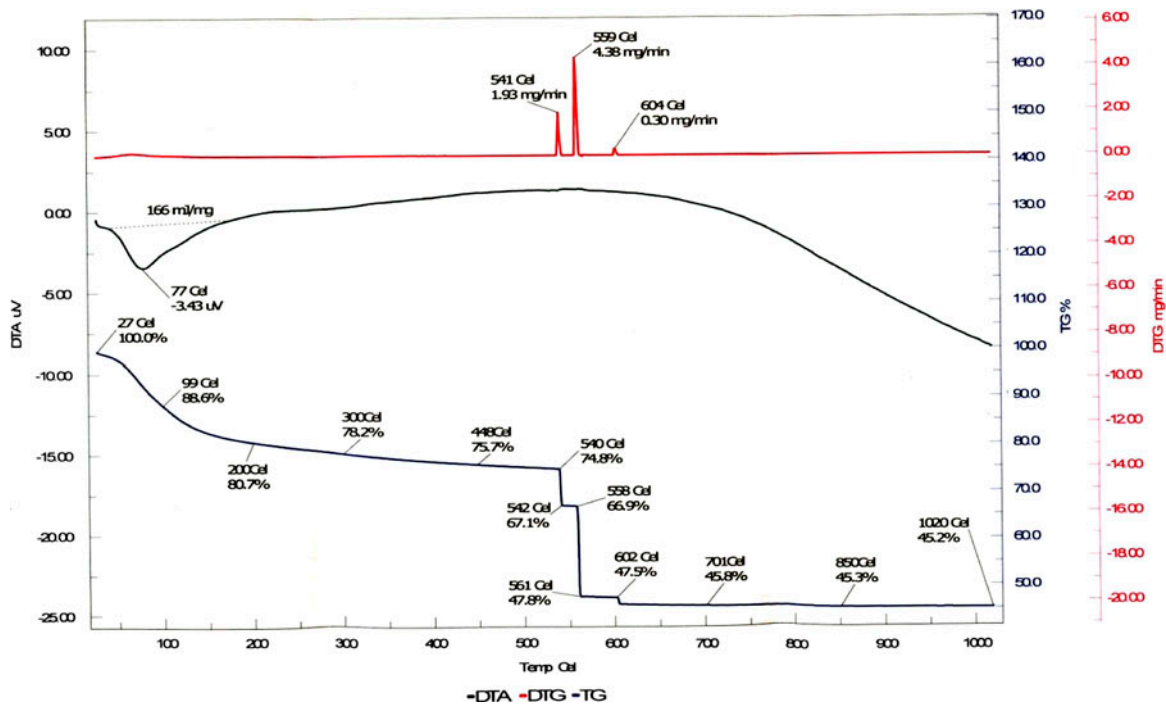


Fig. 2. TGA/DTA curve of SDBS-SnP.

[18]. At further high temperature, the weight of the substance becomes almost constant on heating up to 1,020°C with slight weight losses of 1.7% at 701°C, 0.5% at 850°C and finally 0.1% at 1,020°C. The residual mass of material is due to the formation of tin (IV) oxide (Fig. 2).

SDBS-SnP cation exchanger has been observed to possess higher selectivity towards Cu²⁺, Cd²⁺, Pb²⁺ and Hg²⁺ ions. The K_d -value signifies the ease with which one species sorbs onto a surface. Thus, higher the K_d -value is, the more readily the species are sorbed to the surface. From the Table 4, it is observed that the values of K_d is very high for Hg²⁺ ions as compared to other metal ions in demineralized water, HClO₄ and acetic acid media. Therefore, it can be predicted that Hg²⁺ ions can readily be sorbed onto

SDBS-SnP surface in the aqueous and acidic media of perchloric acid and acetic acid. It is also observed that the k_d value is higher for the metal ion in aqueous solution but its value decreases in the acidic media or on increasing the acid strength due to the competition between the metal ions and hydrogen ions for the binding to the active site of the exchange materials. The high value of k_d for Cu²⁺, Cd²⁺ and Pb²⁺ ions in the presence of respective Na⁺, K⁺, Mg²⁺ and Ca²⁺ ions (Table 5) makes SDBS-SnP a suitable candidate for the removal of transition metal ions in the presence of alkali and alkaline earth metals. The cation exchanger removes Cu²⁺, Cd²⁺ and Pb²⁺ in the presence of 0.1 and .01 M solutions of nitric acid, acetic acid and perchloric acid, respectively, (Fig. 3). The SDBS-SnP removes Cu²⁺, Cd²⁺, Pb²⁺ and Hg²⁺ ions in

Table 4

 K_d values of metals ions on SDBS-SnP cation exchanger in demineralized water and in acidic media

Metal ions	K_d values						
	Demineralized water	0.1 M HNO ₃	0.01 M HNO ₃	0.1 M HClO ₄	0.01 M HClO ₄	0.1 M CH ₃ COOH	0.01 M CH ₃ COOH
Mg ²⁺	446.44	171.42	212.00	346.18	500.85	81.10	120.85
Ca ²⁺	533.30	62.50	128.57	87.72	107.90	52.19	135.32
Ba ²⁺	200.00	183.33	191.50	61.66	87.51	95.82	110.48
Sr ²⁺	500.00	127.77	291.66	65.72	126.42	75.00	113.33
Ni ²⁺	850.00	260.00	733.33	88.58	170.27	102.46	150.02
Fe ²⁺	342.00	81.81	233.33	–	–	–	–
Hg ²⁺	1350.0	220.00	516.20	425.00	960.00	340.00	1060.40

[Metal ion] = 1.0×10^{-3} M, final volume = 20.0 mL, temperature = $25.0 \pm 0.5^\circ\text{C}$.

Table 5

 K_d values of Cu²⁺, Cd²⁺ and Pb²⁺ on SDBS-SnP cation exchanger in the presence of 0.1 M alkali/alkaline earth metals

0.1 M alkali/alkaline earth metal ions	K_d value		
	Cu ²⁺	Cd ²⁺	Pb ²⁺
Na ⁺	261.721	112.71	2429.03
K ⁺	507.906	149.02	1661.79
Mg ²⁺	785.353	555.90	468.11
Ca ²⁺	745.078	207.38	2,293.89

the presence of 0.1 M alkali metals (Na⁺ and K⁺), 0.1 M alkaline earth metals (Mg²⁺ and Ca²⁺) and other transition metal ions (e.g. 0.01 M Zn²⁺, etc.). Thus, these studies show that the material can be used to remove Cu²⁺, Cd²⁺, Pb²⁺ and Hg²⁺ ions from waste water during its treatment in the presence of ambient environmental pollutants. Shao et al. observed that the adsorption capacity of Vulcan XC-72 for Pb²⁺ is increased when grafted with SDBS [19]. They grafted SDBS over carbon (XC-72 carbon) using a plasma technique, and observed that XC-SDBS possessed higher adsorption capacity than XC-72 carbon. They suggested the suitability of XC-SDBS for the immobilization of heavy metal from large volumes of aqueous solutions in environmental pollution cleaning. Pb²⁺ is removed by the negatively charged SDBS molecules by complexation effect, electron attraction and charge neutralization between the dodecyl benzene sulphonate anion headgroup and Pb²⁺ ion [20]. Tagashira et al. extracted Pb²⁺ using SDBS from the mixture of Sn²⁺ [21]. They extracted Pb²⁺ quantitatively in presence of NaCl also. SDBS appears to have a lamellar structure with alternating head-to-head (hydrophilic layer) and tail-to-tail (hydrophobic layer) arrangements. Water molecules and Na⁺ counter ions exist between the heads of the hydrophilic layer. During

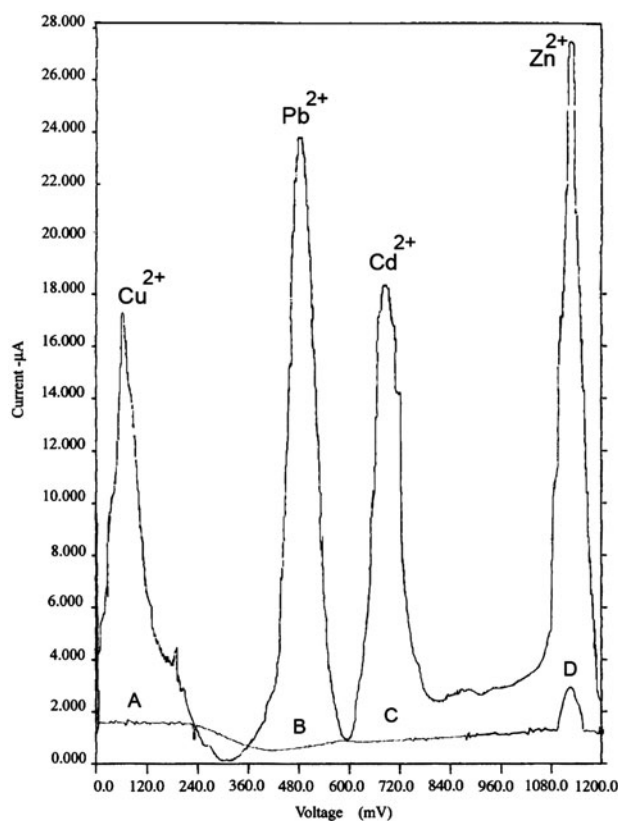


Fig. 3. Differential pulse polarogramme curves for Cu²⁺, Cd²⁺, Pb²⁺ and Zn²⁺ ions before (upper curve) and after (lower curve) passing through the column containing the SDBS-SnP ion exchanger.

the extraction process, Na⁺ ions are replaced by cationic complex of Pb²⁺. The exchange of Na⁺ ions with (Pb(TU)_n)²⁺ ions changes the thickness of the hydrophilic layer. The metal ions are bonded to SDBS molecule through SO group. The bonding between SO group and metal ion is ionic in nature. The incorporation of SDBS into tin (IV) phosphate makes it more

selective for Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions than tin (IV) phosphate alone [5,8]. The adsorption of the ionic species to the ion exchanger is driven by the ionic interaction between the oppositely charged ionic groups in the mobile phase and the functional group available in the cation exchanger (SDBS/SnP/SDBS-SnP). The selectivity possessed in SDBS-SnP for these ions may be attributed to the replacement of sodium

ions from SDBS molecules of SDBS-SnP. This process results into the replacement of Na^+ from the SDBS molecules by Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions and leads to the formation of Cu^{2+} -DBS, Cd^{2+} -DBS, Pb^{2+} -DBS and Hg^{2+} -DBS ion-pairs. The strong electrostatic attractive force is responsible for the binding between the oppositely charged bivalent Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions and dodecyl benzene sulphonate anion (DBS^-). The presence of SDBS in the ion exchanger was confirmed by elemental analysis of the synthesized material. The SDBS molecules coat the tin (IV) phosphate matrix to form an intercalated inorganic-organic fibrous ion exchanger as shown by the SEM photograph in Fig. 4. The cationic exchange material exists in the variable size ranging from 50 to 500 μm .

The IR spectrum of the material in Fig. 5 indicates the presence of phosphate and metaphosphate groups by the appearance of peak at 511.73 cm^{-1} [22]. The appearance of S=O stretching vibration bands was observed at $1,063.35$ and $1,408.60\text{ cm}^{-1}$ [23,24]. The peak at $1,642.74\text{ cm}^{-1}$ represents the water of crystallization and the bands beyond at 3408.13 cm^{-1} correspond to $-\text{OH}$ groups [1,25]. The XRD study of the material has been carried out by using Rigaku Cu $K\alpha$ radiation with the wavelength of $1.54\text{ \AA}$. The absence of defined peak for the material shows that the material is amorphous in nature.

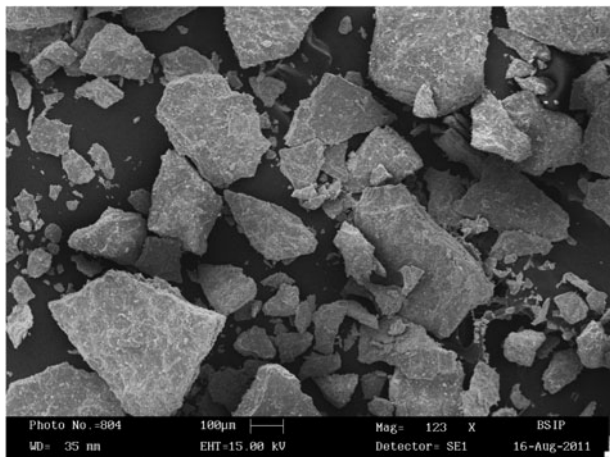


Fig. 4. SEM photograph of SDBS-SnP.

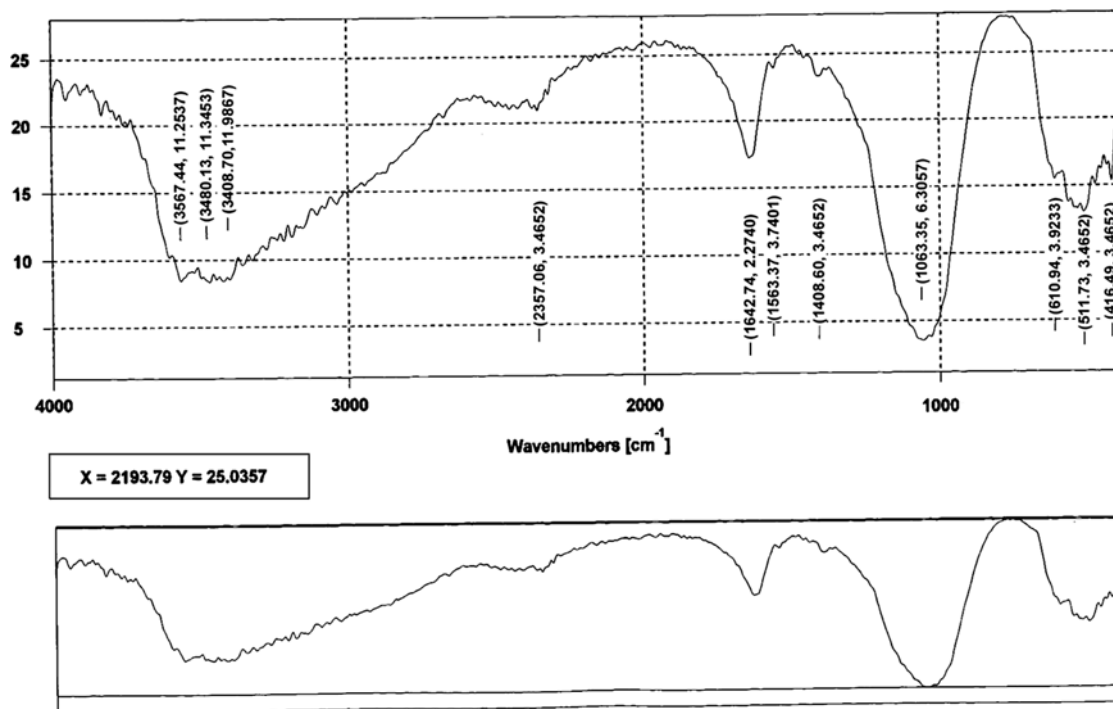


Fig. 5. IR spectrum of SDBS-SnP.

The separation capability of the material has been demonstrated by achieving some binary separations involving Hg^{2+} , viz. Hg^{2+} – Mg^{2+} , Hg^{2+} – Ba^{2+} , Hg^{2+} – Sr^{2+} and Hg^{2+} – Ni^{2+} . The quaternary separations of metal ion were carried out by taking the material in the column. The Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions have been

effectively removed from the mixture containing, Zn^{2+} , Na^+ , K^+ , Ca^{2+} and Mg^{2+} ions in HNO_3 , CH_3COOH or HClO_4 when passed through the thoroughly washed column. The enhanced adsorption of Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} by SDBS–SnP exchanger may be attributed to the formation of ion-pair complexes of surfactant with

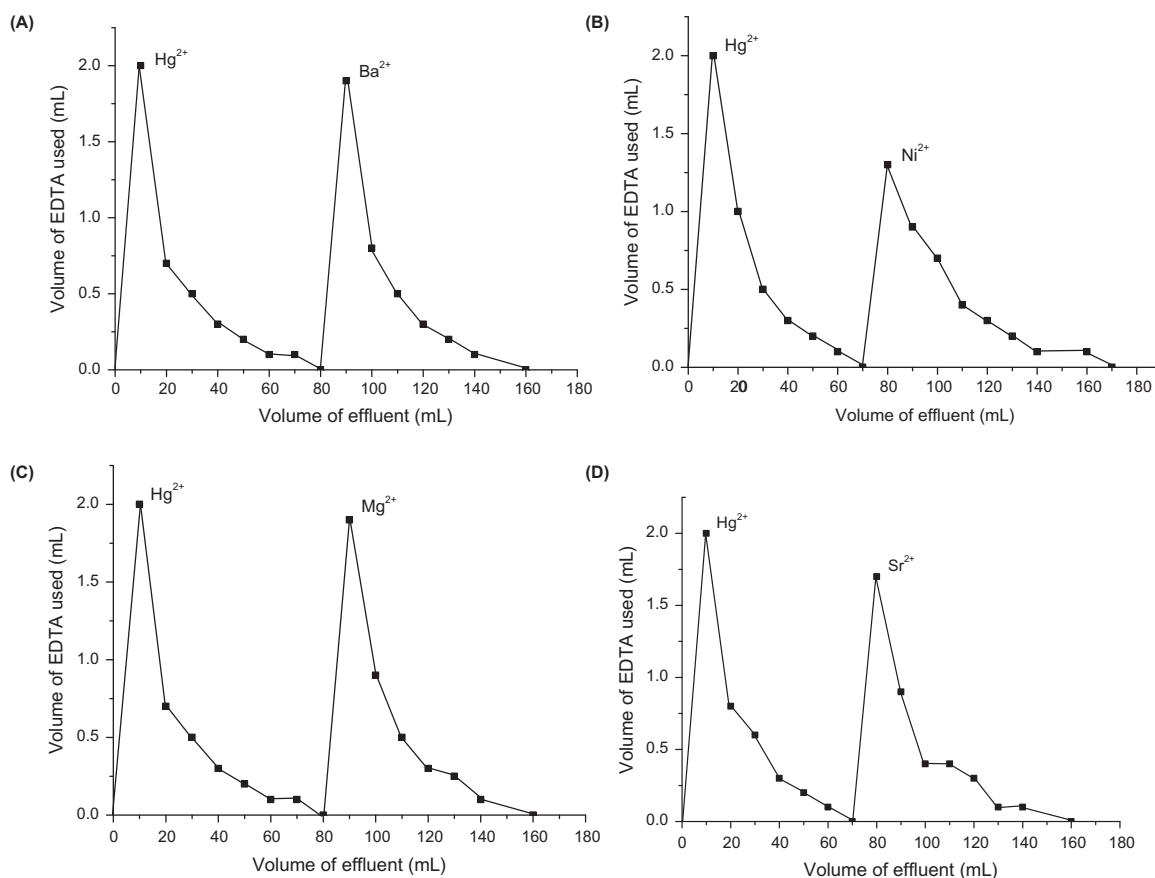


Fig. 6. Chromatogrammes of binary separations of metal ions on SDBS–SnP cation exchanger columns. Eluents 0.1 M CH_3COOH and 0.1 M HClO_4 were for the separation of (A) Hg^{2+} – Ba^{2+} , (B) Hg^{2+} – Ni^{2+} and 0.1 M CH_3COOH and 0.1 M HNO_3 were used for the separation of (C) Hg^{2+} – Mg^{2+} and (D) Hg^{2+} – Sr^{2+} .

Table 6
Binary separations of metal ions achieved on SDBS–SnP cation exchanger column

S. no	Separation achieved	Eluant used	Volume of eluent used (mL)	Amount loaded (μg)	Amount recovered (μg)	Error (%)
1	Hg^{2+}	0.1 M CH_3COOH	70	6852.4	6766.7	–1.25
	Mg^{2+}	0.1 M HNO_3	70	5128.2	5166.6	+0.74
2	Hg^{2+}	0.1 M CH_3COOH	70	6852.4	6732.4	–1.75
	Ba^{2+}	0.1 M HClO_4	60	5226.8	5148.3	–1.50
3	Hg^{2+}	0.1 M CH_3COOH	60	6852.4	6852.4	0
	Sr^{2+}	0.1 M HNO_3	70	4232.2	4126.7	–2.49
4	Hg^{2+}	0.1 M CH_3COOH	60	6852.4	6749.6	–1.50
	Ni^{2+}	0.1 M HClO_4	80	5816.2	5816.2	0

the metal ions and also due to the reduction in interfacial tensions between the solid and liquid phases by amphiphilic nature of surfactant [1]. The sequential elution of the ions from the column depends upon the metal–ligand stability. The elution profiles of metal ion separated are shown in Fig. 6. The weakly retained metal ions were eluted first and strongly retained metal ions were eluted in the last. The separations are quite sharp, and recovery of metal ions was quantitative and reproducible. The results are summarized in Table 6. It is easy to synthesize, durable in nature and capable of removing the Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions from the waste water. It is also cost-effective as the synthesis includes simple method and easily available materials like tin salt, SDBS etc. The high selectivity of material towards Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions will be much helpful in analytical and environmental chemistry for the separation and removal of Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions during the treatment of waste water during its recycling.

4. Conclusion

The synthesized cation exchanger, SDBS-SnP, possessed higher ion exchange capacity (2.20 meq/g) than the tin (IV) phosphate (1.50 meq/g). The addition of SDBS to the matrix of Sn (IV) phosphate improved the mechanical and thermal stability. The cation exchanger is found to be quite selective for the removal of Cu^{2+} , Cd^{2+} , Pb^{2+} and Hg^{2+} ions, and can be used in presence of other impurities like acid, alkalis, alkaline earth and other metal ions. The higher and better selectivity possessed of SDBS-SnP is attributed to the formation of ion-pair between metal ions and surfactant molecules. SDBS-SnP is clean, environment friendly and cost-effective material. The cationic exchange material can be recycled once it is exhausted and will not pose any threat to the environment.

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