Adsorption behavior of tungstate on montmorillonite as a function of pH, ionic strength and competitive anion

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ABSTRACT

A better understanding of adsorption mechanism is vital for the effective reduction of tungsten mobility and potential human health risk such as its suspected link to the childhood leukemia clusters. This study investigated tungstate (WO₄²⁻) adsorption characteristic onto montmorillonite under environmentally relevant solution properties such as the influence of reaction time, solution pH, initial concentration, the competitive anion (PO₄³⁻), and ionic strength. The results of the adsorption isotherm studies suggested that both the Langmuir ($R^2 = 0.9117$) and Freundlich ($R^2 = 0.9913$) equations can be well consistent with WO₄²⁻ adsorption process and the maximal WO₄²⁻ adsorption capacity was 26.73 mmol kg⁻¹. The amount of WO₄²⁻ adsorbed onto montmorillonite strongly dependent on pH and slightly dependent on ionic strength. Specifically, WO₄²⁻ adsorption reached the maximum (17.41 mmol kg⁻¹) at pH 4.15, but becoming negligible (<10%) when pH increase above 9. PO₄³⁻ competed for adsorption sites on montmorillonite with WO₄²⁻. The results of this study indicated that the adsorption mechanism of WO₄²⁻ onto montmorillonite involved ion exchange, inner-sphere surface complexation reaction, and electrostatic attraction. Collectively, our study will aid the understanding of tungsten fate and these results suggest that montmorillonite can be advantageous to the adsorption and recovery of tungsten from real wastewater.

Keywords: Montmorillonite; Tungstate; Adsorption

1. Introduction

Recently, The geochemistry and fate of tungsten has recently gained interest in the scientific and regulatory communities because of its suspected link to the childhood leukemia clusters recently discovered in Nevada, Arizona and California [1–3]. Although, it is no clear evidence that increased concentrations of tungsten leads to these childhood leukemia clusters, much research has recognized that tungsten may be carcinogenic to mammals and toxic to organisms [4–6]. Then, tungsten (*W*) has been recently identified as an

emerging environmental contaminant by the United States Environmental Protection Agency (US EPA) [7].

China is the world's largest *W* producer and consumer. In 2016, the global production of tungsten was 86,400 ton, with over 86% of tungsten (71,000 ton) being produced in China [8]. We have found *W* mining activity in China has contaminated the nearby agricultural soil and led to *W* bioaccumulation in the rice [9]. As anthropogenic activities result in massive amounts of tungsten being released into the environment systems [2], enriching our knowledge of the migration and transformation of *W* in the environmental interfaces is necessary.

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Tungsten persists as tungstate anion or, via polymerization, as a variety of poly-tungstate species, each with varying solubility and soil sorption characteristics [1,3–4,10]. The adsorption behavior of tungsten with soils and clay minerals is the major migration process by which tungsten can be migrated and redistributed in the environment, a comprehensive study of the adsorption mechanism plays an important role in understanding tungsten fate and to remediate tungsten pollution in the environment [10,11].

Montmorillonite is important sink for many oxyanions in the environment and have already been reported to adsorb tungsten (VI) effectively [12,13]. However, existing data for W (VI) adsorption on montmorillionite are relatively limited and incomplete. Hence, the purpose of this research is to investigate the adsorption mechanism of W (VI) onto montmorillonite across varying the solution pH, ionic strength, contact time, initial WO_4^{2-} concentration and competitive anion (PO_4^{3-}). This fundamental study will be helpful for the treatment of soil and water contaminated by tungsten industries and mining.

2. Materials and methods

2.1. Materials and regents

All chemicals used in this study were of analytical grade or higher and used without further purification. Double distilled water was used to prepare solution and clean the sample bottle. All samples were performed in duplicate.

Montmorillonite was obtained from Sigma-Aldrich. Adsorbent properties were characterized by the following methods. X-ray diffraction (XRD) analysis was carried out by a X'Pert PRO MPD machine (PANalytical B.V., Netherlands) with filtered Cu K α radiation (n = 0.1548 nm) operated at 40 kV and 40 mA. Fourier Transform Infrared (FTIR) was performed using a Fourier infrared instrument (Nicolet Nexus 670, America) in pressed KBr pellets. The spectral resolution was sent to 4 cm⁻¹, and 32 scans were collected for each spectrum. The specific surface area (SSA) was surved by the Model QS-7 Quantasorb surface area analyzer (Quantachrom Co., Greenvale, NY).

2.2. Adsorption experiments

The specific experimental steps for WO_4^{2-} adsorption onto montmorillionite and analytical Instruments have been previously reported [14–15]. The detailed experimental parameters list in Table 1. The standard deviation of samples was generally less than 5%.

Table 1

Experimental conditions of tungstate adsorption onto the montmorillonite

3. Results and discussion

3.1. Characterization of montmorillonite

Fig. 1 shows the XRD patterns of montmorillonite sample. The structure of montmorillonite sample is given as $Al_2O_9Si_3$. The peak appears at 26.62 (2 θ) indicates impurity corresponding to quartz in this montmorillonite mineral. The FT-IR spectrum of montmorillonite sample is shown in Fig. 2. The adsorption band at 3,620 cm⁻¹ is due to stretching vibrations of structural –OH groups of montmorillonite. Water in montmorillonite shows strong absorption at 3,440 cm⁻¹ and near 1,638 cm⁻¹ region due to the H₂O-stretching and bending vibrations, respectively [16]. A sharp band at 796 cm⁻¹ confirms quartz admixture in the sample. The very strong adsorption band at 1,089 cm⁻¹ with inflexion near 1,039 cm⁻¹



Fig. 1. XRD pattern of montmorillonite sample.



Fig. 2. FTIR spectrum of montmorillonite sample.

| Experiment | pН | Ionic strength (M NaCl) | Initial W concentration (mM) | Equilibrating time (h) |
|-----------------------------|------|------------------------------|------------------------------|------------------------|
| Kinetic | 5.0 | 0.1 | 0.54 | 1-60 |
| Isotherm | 5.0 | 0.1 | 0.08–1.63 | 48 |
| pH influence | 3–11 | 0.1 | 0.54 | 48 |
| Ionic strength influence | 5.0 | 0.001, 0.005, 0.01,0.05, 0.1 | 0.54 | 48 |
| Competitive anion influence | 5.0 | 0.1 | 0.54 | 48 |

is due to Si-O bending vibration [16,17]. The band at 916 cm⁻¹ is related to Al-Al-OH bending vibrations. The band at 694 cm⁻¹ is due to the deformation and bending modes of the Si-O groups, while the bands at 522 and 469 cm⁻¹ are resulted from Al-O-Si and Si-O-Si bending vibration, respectively [17]. Finally, the SSA of the montmorillonite is 103.85 m² g⁻¹ determined by BET method using N₂.

3.2. Adsorption kinetics of WO_4^{2-} onto montmorillonite

Kinetic study results of WO_4^{2-} adsorption onto montmorillonite is shown in Fig. 3. WO_4^{2-} exhibited rapid reaction during the first 48 h and the reaction rate decreased becoming asymptotic to the time axis after 48 h. Therefore, 48 h was selected as the equilibrium time for WO_4^{2-} adsorption onto montmorillonite. Rapid reaction is often interpreted by scholars as high-affinity sites, while slow reaction as intra-particle diffusion into the mineral defects, the precipitation of ion on the mineral surface, or lower reactive sites [18]. Similar kinetic profile was found for WO_4^{2-} adsorption onto kaolinite [15].

The kinetic data were simulated with three models: the pseudo-first-order and pseudo-second-order model [19], and the intra-particle diffusion model [20]. The kinetic formula is expressed by the following equations, for the pseudo-first-order model:

$$\log(q_{e} - q) = \log q_{e} - \frac{k_{1}}{2.303}t$$
(1)

The pseudo-second-order model:

$$\frac{t}{q} = \frac{1}{k_2 q_e^2} + \frac{1}{q_e} t$$
(2)

The intra-particle diffusion model:

$$q = k_{\rm id} t^{1/2} + C \tag{3}$$



Fig. 3. Influence of reaction time on the tungstate adsorption onto montmorillonite, I = 0.1 M NaCl, pH = 5.0 ± 0.1 , $T = 25^{\circ}C \pm 2^{\circ}C$, and $C_{\text{tungstate initial}} = 0.54$ mM.

In Eqs. (1)–(3), *q* and *q*_e (mmol kg⁻¹) are the amounts of WO₄²⁻ adsorbed at the time, *t* (h) and at equilibrium, respectively, *k*₁ (h⁻¹) is the pseudo-first-order rate constant for WO₄²⁻ adsorption, *k*₂ (kg mmol⁻¹ h⁻¹) is the pseudo-second-order rate constant (kg mmol⁻¹ h⁻¹), *k*_{id} (mmol kg⁻¹ h^{-1/2}) is the relevant rate constant for WO₄²⁻ adsorption and *C* is the intercept.

Plots of the three kinetic model of WO₄^{2–} adsorption onto montmorillonite are presented in Fig. 4. Comparing with the pseudo-first-order model, the diagram of t/q_i vs. t (Fig. 4(b))



Fig. 4. Kinetic simulation of tungstate adsorption onto montmorillonite: (a) the pseudo-first-order model, (b) the pseudo-second order model, (c) the intra-particle diffusion model.

indicates that the pseudo-second-order model ($R^2 = 0.999$) will better simulate the kinetics of WO₄²⁻ adsorption onto montmorillonite than pseudo-first-order model ($R^2 = 0.944$). Value of k_1 calculated from linear graph was 1.38×10^{-2} h⁻¹, which is similar with WO₄²⁻ adsorption onto Oxisols (K_{ad} 1.10 $\times 10^{-2}$ h⁻¹ at the initial WO₄²⁻ concentration 0.04 mM) [15] and kaolinite (K_{ad} 1.05 $\times 10^{-2}$ h⁻¹ at the initial WO₄²⁻ concentration 0.27 mM) [14]. The value of k_1 was varied with different initial WO₄²⁻ concentration and different materials. Plot of q vs. $t^{1/2}$ (Fig. 4(c)) followed three distinct phases of adsorption process, initial curved portion followed by linear and a plateau. The initial curved portion is resulted from the bulk diffusion, the linear portion of the solid-state diffusion and the plateau to the relative equilibrium. The properties of graph show that the uptake of WO₄²⁻ by montmorillonite is controlled by surface adsorption and intra-particle diffusion. The rate con-

3.3. Adsorption isotherm

of the curve was 0.171 mmol kg⁻¹ h^{1/2}.

The adsorption process of WO_4^{2-} onto montmorillonite was modeled by the Langmuir and Freundlich equation. The Langmuir model [21] assumes that monolayer adsorption occurs on a finite number of homogenous surfaces without any interaction between adsorbed ions, and the equation is represented by the following:

stants value (k_{id}) obtained from the slope of the linear portion

$$\frac{C_e}{q_e} = \frac{C_e}{q_m} + \frac{1}{q_m K_L} \tag{4}$$

where C_e (mmol L⁻¹) is the equilibrium concentration of WO₄²⁻ in solution, q_e (mmol kg⁻¹) is the WO₄²⁻ adsorption amount, q_m (mmol kg⁻¹) is the maximal adsorption capacity, and $K_{\rm L}$ (L mmol⁻¹) is the constant related to the binding energy.

The Freundlich isotherm [22] is commonly used for heterogeneous, multilayer adsorption, and the equation can be expressed as:

$$q_e = K_F C_e^{\frac{1}{n}} \tag{5}$$

where C_e (mmol L⁻¹) is the equilibrium concentration of WO₄²⁻ in solution, q_e (mmol kg⁻¹) is the WO₄²⁻ adsorption amount, K_F (mmol¹⁻ⁿ kg⁻¹ Lⁿ) is the Freundlich constant related to the adsorption intensity, and *n* is the heterogeneity factor.

Fig. 5 shows the adsorption isotherms of WO₄²⁻ onto montmorillonite and fits of the Langmuir and Freundlich equation. Based the correlation coefficients, the Freundlich isotherm describes the experimental data better than Langmuir equation (Table 2). The WO₄²⁻ maximal adsorption capacity was 26.73 mmol kg⁻¹ and equilibrium constant $K_{\rm L} = 0.0793$ L mmol⁻¹, which was consistent with the previous research [12,13,23]. Tuna and Braida [12] found the maximal predicted WO₄²⁻ capacity of montmorillonite was 9.89 mmol kg⁻¹. We believed experimental conditions and the different characteristic of adsorbent can account for this discrepancy. Our previous research founded that both the Langmuir model and the Freundlich model were fitted to the WO₄²⁻ adsorption onto the Oxisols, which the maximal adsorption capacity of WO₄²⁻ was 10.09 mmol kg⁻¹ and the distribution coefficient 12.6 L g⁻¹ [15]. Xu et al. [24] found that goethite adsorbed more tungstate than montmorillonite with the maximal capacity of 225.7 mmol kg⁻¹ and the distribution coefficient 159.1 L g⁻¹. The difference of montmorillonite characteristics (i.e. specific surface area, surface charges) leads to varies of the maximum WO₄²⁻ adsorption amount.

3.4. Effect of pH

Solution pH can affect the adsorption of WO42- onto montmorillonite through multiple pathways such as affecting surface site protonation, and WO_4^{2-} complexation and hydrolysis. Effect of pH on the adsorption of WO_4^{2-} onto montmorillonite is illustrated in Fig. 6. As shown in the figure, it is clear that the amount of adsorbed WO_4^{2-} decreased with increasing solution pH. More specifically, the amount of adsorbed WO₄²⁻ reached the maximum (17.41 mmol kg⁻¹) at equilibrium pH around 4.15, decreased steadily in the pH range from 5.0 to 7.0 and became negligible (<10%) when pH increase above 9.0. This is consistent with previous study that $WO_{\scriptscriptstyle\! A}^{\ 2-}$ adsorption is pH dependent with increased adsorption occurring at acidic pH and little at pH>9 [12,25]. One possible explanation is the protonation state of clay surface functional groups. Also, the aqueous speciation of tungsten changes with pH is also another issue, which is influenced by the pKa



Fig. 5. Adsorption isotherm of tungstate onto montmorillonite clay, I = 0.1 M NaCl, pH = 5.0 ± 0.1, $T = 25^{\circ}$ C ± 2°C, and $C_{\text{tungstate initia}} = 0.08$ to 1.63 mM.

Table 2

Langmuir and Freundlich constants of tungstate adsorption on montmorillonite

| Model | Langmuir | Freundlich |
|---|----------|------------|
| $K_{L'}$ L mmol ⁻¹ | 0.0793 | _ |
| Q _{max'} mmol kg ⁻¹ | 26.73 | — |
| $K_{\mathbf{p}'} \operatorname{mmol}^{1-n} \operatorname{kg}^{-1} \operatorname{L}^{n}$ | — | 26.68 |
| Ν | — | 3.60 |
| R^2 | 0.9117 | 0.9913 |
| SE | 2.93 | 0.92 |

value [26]. The two pKa values for H_2WO_4 (pKa1 = 3.62 [27], pKa2 =5.08 [28]) bracket a wider pH range which promotes the adsorption of WO_4^{2-} on montmorillonite. The dimeric tungstate ions (WO_4^{2-}) occurs in alkaline environemnts,



Fig. 6. Influence of pH on tungstate adsorption onto the montmorillonite, I = 0.1 M NaCl, pH = 3.0 ± 0.1 to 11 ± 0.1 , $T = 25^{\circ}C \pm 2^{\circ}C$, and $C_{tungstate initial} = 0.54$ mM.

whereas a number of thermodynamically stable and unstable polymerized tungstate forms coexist in acidic solution as in Fig. 7 [1,29–31]. Some microscopic spectral evidences (i.e. XAS and ATR-FTIP) for the effect of pH on WO₄²⁻ speciation change have been reported [11,31,32]. Specifically, the formation of polymeric of WO₄²⁻ under a wide pH range (i.e. pH 4–8) decreased the WO₄²⁻ adsorption amount on mineral surface, and thereby led to easily tungsten mobilization in the environment [11,31,32]. Another possible explanation is that an increase of OH⁻ ions in basic solution will compete with WO₄²⁻ for the adsorption sites and result in a decrease in WO₄²⁻ adsorption. So the adsorption mechanism of WO₄²⁻ onto montmorillonite involves more than one mechanism such as polymerization at low pH and adsorption.

Positive identification of adsorbed WO₄²⁻ species was provided using the XRD and FTIR technique. In Fig. 8(a) XRD pattern is presented for the sorbent, as well as for the sorbent after WO₄²⁻ sorption at pH 5.0. Following WO₄²⁻ sorption, the loaded sorbent had the same structure of montmorillonite. But three new bands appearing at 20°, 26°, and 50° could be attributed to the formation of new precipitate, which indicates surface complexation. FTIR spectrophotometer result of montmorillonite, both before and after WO₄²⁻ adsorption, shows several frequency shifts (Fig. 8(b)).These shifts are important indicators of molecular interactions and reflect the effect of the surface complexation between adsorption sites and WO₄²⁻ species rather than solid phase precipitation.



Fig. 7. Tungsten speciation as a function of pH (based on references [1,29–31]).



Fig. 8. (a) X-ray patterns of montmorillonite and montmorillonite after tungstate adsorption, (b) FTIR spectra of montmorillonite and montmorillonite after tungstate adsorption.

3.5. Effect of ionic strength

Ionic strength plays a role in the WO₄²⁻ adsorption onto montmorillonite (Fig. 9.). It was illustrated that the amount of adsorbed increased steadily from 35.2% to 62.0% with the increase of ionic strength. One definitive explanation is that the increase of solution ionic strength for clay systems results in the shielding of the net negatively-charged surface electric field, and thereby reduce the repulsive force to anion [34,35]. This effect allows more WO_4^{2-} to adsorb onto the montmorillonite surface at high ionic strength conditions as compared with low ionic strength conditions. Another possible explanation is the formation of inner-sphere WO_4^{2-} surface complexes, because higher ionic strength may facilitate the transformation of outer-sphere complex into inner-sphere complex and hence might increase total adsorption amount [33]. Increased WO42- adsorption at high ionic strength is consistent with previous research of WO42- adsorption onto pyrite and boehmite, where it was suggested that the increased WO₄²⁻ adsorption may be caused by the effect of coadsorption of cations (i.e., Na⁺) and WO₄²⁻ [11,36]. Thus, the effect of ionic strength for WO₄²⁻adsorption onto the clay colloid surface may include the promotion of the inner-sphere adsorption process and the weakness of the positive electrostatic field at the mineral surface and finally increased the total WO²⁻ adsorption.

3.6. Effect of competitive anions

The influence of competitive anion PO_4^{3-} on the adsorption of WO_4^{2-} onto montmorillonite was investigated using the mol ratio P/W from 0 to 10 (Fig. 10). As shown in Fig. 10, tungstate adsorption onto montmorillonite was strongly affected by phosphate. Without adding phosphate, the amount of adsorbed WO_4^{2-} was 15.83 mmol kg⁻¹, but the adsorption of WO_4^{2-} gradually decreased with the increase of the phosphate concentration. However, the final decrease amount of adsorbed WO_4^{2-} (14.30 mmol kg⁻¹) is less than the final increase amount of adsorbed PO_4^{3-} (113.30 mmol kg⁻¹) with the change of the mol ratio P/W



Fig. 9. Influence of ionic strength on tungstate adsorption onto the montmorillonite, I = 0.001 to 0.1 M NaCl, pH = 5.0 ± 0.1, $T = 25^{\circ}\text{C} \pm 2^{\circ}\text{C}$, and $C_{\text{tungstate initial}} = 0.54$ mM.



Fig. 10. Influence of phosphate on the adsorption of tungstate. I = 0.1 M NaCl, pH = 5.0 ± 0.1, $T = 25^{\circ}\text{C} \pm 2^{\circ}\text{C}$, $C_{\text{tungstate initial}} = 0.5 \text{ mM}$, and $C_{\text{phosphate}} = 0.05$ to 5.0 M.

from 0 to 10, which suggesting that the specific adsorption of WO₄²⁻ onto montmorillonite surface and the stronger affinity of montmorillonite for PO43- compared with the affinity for WO42-. Mulcahy et al., [37] concluded that alumina contained loosely and tightly bound surface sites for WO₄²⁻ adsorbed. Therefore, it can be explained that the montmorillonite might have small adsorption sites common to WO₄²⁻ and PO₄³⁻ anions and large adsorption species specific to WO_4^{2-} or PO_4^{3-} anions. PO_4^{3-} affecting adsorption of WO₄²⁻ by competing for a few percent available surface sites has been reported on natural soil and other minerals (such as ferrihydrite, kaolinite and oxisols) [15,38]. Another interpretation for the decreased adsorption of WO₄²⁻ is that WO₄²⁻ polymerizes with PO_4^{3-} and produces polyoxometalates (POMs) such as phosphotungstate $PW_{12}O_{40}^{3-}$ in solution [31]. So PO_4^{3-} reduces WO_4^{2-} adsorption onto montmorillonite by competing for limited surface adsorption sites and altering the WO₄²⁻ solution speciation in solution.

4. Conclusion

Recently, interest in tungsten (W) geochemistry and transformation has increased due to its suspected link to the childhood leukemia clusters. A comprehensive understanding of adsorption mechanism is vital for the effective reduction of tungsten mobility and potential human health risk. However, existing data are relatively limited and incomplete. In this study, the results have confirmed that tungstate adsorption onto montmorillonite is an important factor influencing the tungsten transformation in natural environments. Montmorillonite can be used as an important scavenger for removing of tungsten from aqueous solution by adsorption process. Specifically, the kinetic adsorption data of tungstate onto montmorillonite was well simulated by a pseudo-second-order model and suggested the rate-controlling steps of tungstate was intra-particle diffusion and rapid out-sphere adsorption. The adsorption isotherm data was fitted into both Langmuir and Freundlich model. The amount of tungstate adsorption onto montmorillonite decreased with pH increasing but increased with ionic strength. Phosphate competed with tungstate for adsorption sites onto montmorillonite. These results demonstrate that the mechanism for tungstate adsorbed onto montmorillonite was electrostatic attraction and inner-sphere surface complexation reaction and influenced by many factors such as intrinsic properties of adsorbent, tungsten concentration, and speciation, solution pH, ionic strength, and the reaction time. This study investigated a single adsorbent and simple composition of solutions. The natural environment is a very complex system, which could complicate the transformation and migration of W in environment. Further efforts are required to improve knowledge of W environmental chemistry, and its environmental transformation and exposure.

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